# Agenda

#### Energy conservation, conversion, and transformation

- Potential energy, kinetic energy, work, and power Variable force, chemical rearrangement energy (Enthalpy) Examples
- Kinetic energy transfer,

Dissipation, randomization and spontaneous processes Examples of thermal motion, Maxwell-Boltzmann distribution

• Transfer of thermal energy (heat)

Conduction, convection, radiation (cooling) Internal energy, equivalence of work and heat Basic (First Law & Second) Laws of Thermodynamics, Entropy and spontaneous processes.

 Thermal engines Ideal Carnot processes Real gases/substances

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## Basic Laws of Statistical Thermodynamics

**Consider complex systems: Many degrees of freedom** (=many particles, particles with complex structure, complex internal energy states, complex materials with different phases,.., chaos)

**Observation of dissipative phenomena:** Excitation of complex systems initiates evolution toward maximum dissipation (Equilibrium)

Statistical Thermodynamics: <u>Physics of equilibration & equilibrium</u>

- O) Systems in contact equalize mean internal (kinetic) energies,
   → temperatures equalize.
   "Canonical & grand canonical" ensembles (of many ident. systems).
- **1)** Energy (of system plus surroundings) is conserved.
- 2) Complex systems evolve spontaneously toward state of maximum randomness (complexity) → Measure=Entropy.
- **3)** There exists an absolute "zero point" of energy for any system: energy and complexity are at a minimum (@ absolute T=0 K).

#### Randomization: Spontaneous Dissolution of Cluster

Transitions from one s.p. state (pixel<sub>i</sub>) to another (pixel<sub>j</sub>) are micro-reversible (unlikely).



S = State Function; Boltzmann (1877)

## Randomization: Spontaneous Dissolution of Cluster

Transitions from one s.p. state (pixel<sub>i</sub>) to another (pixel<sub>j</sub>) are micro-reversible (unlikely).



2. Law of TD: Entropy increases in spontaneous processes  $\Delta S/\Delta t > 0$ 

## Entropy of Mixing: Example

One mole each of two equivalent ideal gases,  $A=O_2$  and  $B=H_2$ , in their respective halves of a separated container at  $P_A = P_B = 1$  atm,  $T_A = T_B = 298K$ 

s.p. spaces  $\sigma_A \propto V_A$ 

When partition is removed, the gases will mix.

No change in energy  $\Delta q = 0$ 

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Universal Gas Constant R=8.31*J/mol·K* 

Phenomen 1&2. LTD

Information on s.p. configuration space from EoS Ideal gases  $P \cdot V = n \cdot R \cdot T \rightarrow \varpi_{A,B} \propto V_{A,B} \propto n_{A,B}$ 

Total n = 2 moles; Mole fractions:  $n_A/n = n_B/n = 0.5$ .  $\rightarrow$  probabilities are  $p_A = p_B = 0.5$  also in state space

→ "Entropy of Mixing"

$$\Delta S_{mix} = -nR\left\{\frac{n_A}{n} \cdot Ln\left(\frac{n_A}{n}\right) + \frac{n_B}{n} \cdot Ln\left(\frac{n_B}{n}\right)\right\} = -2R\left\{0.5 \cdot Ln(0.5) + 0.5 \cdot Ln(0.5)\right\} = 11.5 \text{ J/mol} \cdot \text{K} > 0$$

Entropy is gained ←→ mixing occurs spontaneously.

 $\Delta S \ge \frac{\Delta q}{T}$  in spontaneous processes

Mixed gases are difficult to unmix (costs energy)!

# **EoS: Entropy of Mixing**

#### **Separated Gases**



**Mixed Gases** 



S - gain by individual gas components  $\Delta S_i = n_i \cdot R \cdot Ln\left(\frac{V}{V_i}\right) > 0 \qquad n_i = number \text{ of moles } i$ 

Entropy is extensive (additive).  $\rightarrow$  conponents add  $\Delta S = -R \cdot \sum_{i} n_{i} \cdot Ln\left(\frac{V_{i}}{V}\right) > 0 \qquad S \nearrow$ 

total moles 
$$n = \sum_{i} n_{i} \rightarrow \Delta S = -n \cdot R \cdot \sum_{i} \left(\frac{n_{i}}{n}\right) \cdot Ln\left(\frac{V_{i}}{V}\right)$$

Relative abundance (probability for) particle type i

 $p_{i} = \frac{n_{i}}{n} = \frac{V_{i}}{V} < 1$   $\Delta S = -n \cdot R \cdot \sum_{i} p_{i} \cdot Ln p_{i}$  *n* moles  $\Delta S = -N \cdot k_{B} \cdot \sum_{i} p_{i} \cdot Ln p_{i}$ 

Can use other "State Functions" to calculate entropy, all related by EoS

#### Thermodynamics: Ideal-Gas Equations of State EoS





Robert Boyle, Guillaume Amontons, Gay-Lussac, Dalton,... Response of dilute gases of specified amounts (#moles = *n*, *Avogadro*)

Boyle's Law  $P(V) \propto 1/V$  or  $P \cdot V = const(n,T)$ 

Amontons' (Gay – Lussac's) Law  $P(T) = P(0) \cdot [1 + \alpha \cdot T_c] \propto T$ 

Charles' Law  $V(T_c) = V(0^\circ C) \cdot [1 + \alpha \cdot T_c] \rightarrow V(T) \propto T$  (Kelvin) Compression

 $\alpha \approx 3.66 \cdot 10^{-3} / ^{\circ}C \approx 1/273^{\circ}C \rightarrow absolute temperature T$ 

#### EoS of Ideal Gases

Isentropic T=const.

$$P \cdot V = n \cdot R \cdot T = N \cdot k_{\scriptscriptstyle B} \cdot T$$



Polytropic EoS Polytrope coefficient  $\gamma = C_P/C_V$  $T \cdot V^{\gamma-1} = const$ Polytropic EoS

2 Specific Heats @P = const. or V = const.Thermal energy content  $Q = C_{P,V} \cdot T$  Empirical Law

#### Reversible Circular Processes on EoS Hyperplane



 $\underset{W. Udd}{\mathbb{R}_{h \neq d} 8.3145 \text{ J/mol} \cdot \text{K}}{\text{times}} \rightarrow \text{Cyclic thermal engine}$ 

## Entropy and Energy at Equilibrium: Ideal Gases

Many systems in mutual contact, provide heat energy E just to System#1 (E = E - total)  $\rightarrow$  eventual stationary state – maximum probability – all acquire same temperature T  $\left(\frac{1}{\Omega}\frac{d\Omega(E)}{dE}\right) = \left(\frac{1}{\Omega}\frac{d\Omega(E)}{dE}\right) = \left(\frac{1}{\Omega}\frac{d\Omega(E)}{dE}\right) = \left(\frac{1}{\Omega}\frac{d\Omega(E)}{dE}\right) \cdots \Rightarrow \frac{d\Omega(E)}{QdE} = \frac{d\ln[\Omega(E)]}{dE} = \underline{Const}(E)$ Independent of material, size, shape, amount  $\rightarrow$  Function Const depends on total energy E supplied to one of the systems as heat. Dimension [Const(E)] = 1/energy. Obvious & simplest *intensive energy* variable = temperature T $\rightarrow$ System energy content of an ideal gas (N particles):  $P \cdot V = N \cdot k_B \cdot T$ Adopt *intensive* energy variable  $\rightarrow$  Energy per particle  $\frac{E}{N} \propto \frac{P \cdot V}{N} = k_B \cdot T$ Adopt intensive function S with  $\frac{dS}{dE} = \frac{1}{\Omega} \frac{d\Omega(E)}{dE} = \frac{d}{dE} k_B Ln\Omega(E) \propto \frac{1}{T}$  Simplest form compatible S extensive  $S(E) = k_B Ln \Omega = \sum_{A} + \frac{E}{T} \rightarrow Distributed heat energy E = T \cdot S$ integration constant =0Heat absorption / emission by system @equil T :  $\Delta \langle E \rangle = \Delta q \rightarrow \Delta S = \frac{\Delta q}{T}$ 

## Thermal Engine: Expansion-Compression Cycles

Ideal-gas system (N particles) absorbing external heat (q>0) can produce mechanical work (w<0) on surroundings. Continuous operation requires cyclic process (in p-V-T).  $\rightarrow$  Needs good contacts to heat bath  $@T_1$  and heat sink  $@T_2 \rightarrow$  reversible processes



In one cycle the gas absorbs net heat energy and does the net work,

 $w = w_1 + w_2 = -q = C_V \cdot [T_2 - T_1]$ 

Not all absorbed heat is converted, some must be dumped as waste heat.

Isothermal expansion at T<sub>1</sub>=const.
 Isochoric decompression at V<sub>2</sub>=const.,
 Isothermal compression at T<sub>2</sub>=const.
 Isochoric compression V<sub>1</sub>=const.,

Sign convention: Internal energy gain or loss

→ Work-Heat Balance:			
1-2 gas does wo	rk -w <sub>1</sub>	= q₁; <mark>∆l</mark>	J = 0
2-3 gas is cooled	> p t	0; <u>A</u>	J < 0
3-4 gas is comp	ressed w <sub>2</sub> =	= - q <sub>2</sub> ; ∆	U = 0
4-1 gas is heate	d q >	0; 🛆	U > 0
Total internal energy: $\Delta U = 0$ (cyclic)			
Total heat absor	bed: $q = a$	ק₁+q₂ <b>=-и</b>	<i>י</i> > 0
Total work by er	ngine : <b>w =</b>	$w_1 + w_2 <$	< 0

#### Carnot Engine Cycles



Energy balance:  $w = q_1 + q_2 > 0$ on isothermal portions: w+q=0 Adiabatic works cancel 1

$$\boxed{q_1} = -w_1 = \int_{V_1}^{V_2} p \, dV = R \cdot \boxed{T_1} \cdot \ln\left(\frac{V_2}{V_1}\right) > 0$$

$$\boxed{q_2} = -w_2 = \int_{V_3}^{V_4} p \cdot dV = R \cdot \boxed{T_2} \cdot \ln\left(\frac{V_4}{V_3}\right) < 0$$

Reversible adiabatic exp./compr.:  $\Delta S = q/T = 0$ since q = 0. Irreversible adiabatic exp./compr.:  $\Delta S \neq 0$ .

Adiabatic (q = 0) EoS  $T \cdot V^{\gamma-1} = const$   $\gamma = c_p/c_v$ Adiab. expansion/compr.  $\rightarrow V_4/V_1 = V_3/V_2$  $\rightarrow V_{4}/V_{3} = V_{1}/V_{2}$ 

 $T_h \rightarrow T_c = T_2$ 

"Entropy"  $\left| \frac{q_1}{T_1} = -\frac{q_2}{T_2} \right| = -\Delta S_2 = \Delta S_1$ Entropy is conserved in reversible *cyclic processes*:  $\Delta S_1 + \Delta S_2 = 0$ .  $\rightarrow$  S = state function (descriptor)

For any process:  $\Delta S_{A \to B} \geq \frac{q_{A \to B}}{T}$ = sign for reversible  $A \rightarrow B$  only.

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V

#### Efficiency of Carnot Engines



Efficiency of an ideal Carnot engine

$$\mathcal{E}_{C} = \frac{-w}{q_{h}} = \frac{q_{h} + q_{c}}{q_{h}}$$
$$\mathcal{E}_{C} = 1 + \frac{q_{c}}{q_{h}} = 1 - \frac{T_{c}}{T_{h}} \xrightarrow{T_{h} \to \infty} 1$$

- Efficiency of a realistic Carnot-type engine must be lower than  $\epsilon_{\rm C}$ .
- All engines based on *pV* processes can be simulated by a combination of Carnot processes.
- No thermodynamic (*pV*) engine can have an efficiency larger than  $\epsilon_{\rm C}$ .

Typical thermal engines have efficiencies of  $\varepsilon_{\text{therm}} \sim 0.3$ .

# Thermal (Coal) Power Plant

Fuel  $\rightarrow$  Combustion Heat  $\rightarrow$  Steam  $\rightarrow$  Expansion Work  $\rightarrow$  Electromagnetic Work  $\rightarrow$  Electrical Power



U.S. now: 600 *large* coal-fueled electrical power plants (0.5-1GW), many (~10<sup>3</sup>) smaller units. Predictions (BAU) by 2030: +150 (?) ( $\approx$ 100 GW), 12 now under construction. Newer units: combined cycle (IGCC), power/heat co-generation.  $\rightarrow$  convert to nG ?

# End of Work, Energy, & Power II

# **Geothermal Power**

The Party

#### U.S. Geothermal Resources



Most of the geothermal power plants in the United States are in western states and Hawaii, where geothermal energy resources are close to the earth's surface. California generates the most electricity from geothermal energy. The Geysers dry steam reservoir in Northern California is the largest known dry <sup>W. Udo So</sup>steam field in the world and has been producing electricity since 1960. Worldwide simplest (conventional/ancient) direct use: building/district heating. Utility: Geothermal electrical power plants, Residential: geothermal heat pumps, A/C



Generating technology: Inject fresh water (hydro fracturing), extract hot water  $\rightarrow$  steam  $\rightarrow$  drive steam turbines & electric generators



From H. Kennedy, 2020; citing Augustsson & Flovenz, 2--4 W. Udo Schröder, 2023

#### Extract Geothermal Heat: Carnot Engines

Cyclic Carnot process **at constant entropy**  $\Delta S \rightarrow \text{work } \boldsymbol{w} = -(\boldsymbol{q}_h + \boldsymbol{q}_c) < \boldsymbol{0}$  on environment powered by transferring heat from hot to cold sink  $(T_h \rightarrow T_c)$ .  $\rightarrow \text{Refrigerator}$ 

**Ideal Gas:** Every cyclic pV engine can be modeled as Carnot process.

$$T_{h}$$

$$q_{h} = \Delta S \cdot T_{h}$$

$$p_{\Delta S} = const$$

$$q_{c} = -\Delta S \cdot T_{c}$$

$$q_{c} = -\Delta S \cdot T_{c}$$

Efficiency of an ideal Carnot engine

$$\varepsilon_c = 1 + \frac{q_c}{q_h} = 1 - \frac{T_c}{T_h}$$

- $\epsilon_{C}$  is maximum efficiency of a realistic Carnot-type engine.
- All engines based on *pV* processes can be simulated by a combination of Carnot processes.
- No thermodynamic (*pV*) engine can have an efficiency larger than  $\epsilon_{\rm C}$ .

**Reversing Carnot process** implies sign changes of heat energies and work  $\rightarrow$  External work w > 0 done on system can transfer heat from a cold reservoir to a hot reservoir  $(T_c \rightarrow T_h)$ . Thermal engine efficiencies  $\varepsilon_{\text{therm}} \sim 0.3$ .

#### Entropy and Heat Flow in Reverse Carnot Process



 $T_h$   $q_h = -\Delta S \cdot T_h$   $-w = q_h + q_c =$   $= \Delta S \cdot (T_c - T_h)$   $q_c = +\Delta S \cdot T_c$   $T_c$ 

Maximum efficiency  $\eta_c = 1 - \varepsilon_c = \frac{q_c}{q_h} = \frac{T_c}{T_h}$ 

Entropy  $\Delta S$  with heat  $q_c = \Delta S \cdot T_c$  from the  $T_c$  reservoir preheats the colder  $(T_h)$  working fluid/gas, which enters an externally powered compressor. The compressor **does work** on the fluid, raising its temperature to  $T_h$ . Heat energy  $\Delta S \cdot T_h$  is then transferred to the  $T_h$  heat reservoir.

Analog: Stream of water  $\Delta M$  from a river carries energy  $\Delta M \cdot g \cdot h_1$ , enters an externally powered pump that lifts  $\Delta M$  by  $(h_2 - h_1)$  to the reservoir head at energy  $\Delta M \cdot g \cdot h_2 > \Delta M \cdot g \cdot h_1$ .

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#### Entropy and Heat Flow in Reverse Carnot Process





Entropy  $\Delta S$  with a heat energy of  $\Delta S \cdot T_c$  from the  $T_c$  reservoir warms the colder working fluid, which enters an externally powered compressor. The compressor **does work** on the fluid, raising its temperature to  $T_h$ . The heat energy of  $\Delta S \cdot T_h$  can then be transferred to the heat reservoir.

Analog: Stream of water  $\Delta M$  from a river carries energy  $\Delta M \cdot g \cdot h_1$ , enters an externally powered pump that lifts  $\Delta M$  by  $(h_2 - h_1)$  to the reservoir head at energy  $\Delta M \cdot g \cdot h_2 > \Delta M \cdot g \cdot h_1$ .

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### **Residential Heat Pump**



#### https://www.energy.gov/eere/geothermal/electricity-generation



#### U.S. Geothermal Power Electricity Generation 2022

State share of total U.S. geothermal electricity generation		Geothermal share of total state electricity generation	
California	69.5%	5.8%	
Nevada	24.2%	9.6%	
Utah	2.7%	1.2%	
Hawaii	1.8%	3.2%	
Oregon	1.2%	0.3%	
Idaho	0.5%	0.5%	
New Mexico	0.3%	0.1%	

<u>2022</u>: US produced about 17 TWh (17 billion kWh) = 0.4% of total U.S. utility-scale electricity generation. (Utility-scale power plants: capacity  $\geq$  1 megawatt (1MW<sub>e</sub>) of electricity generation)

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ENERGY

Office of ENERGY EFFICIENCY & RENEWABLE ENERGY

**GEOTHERMAL TECHNOLOGIES OFFICE** 

# Fiscal Years 2022–2026 MULTI-YEAR PROGRAM PLAN

**Strategic Goal 1:** Drive toward a carbon-free electricity grid by supplying 60 gigawatts (GW) of Enhanced Geothermal Systems and hydrothermal resource deployment by 2050.

**Strategic Goal 2:** Decarbonize building heating and cooling loads by capturing the economic potential for 17,500 Geothermal district Heating installations and by installing GHPs in 28 million households nationwide by 2050.

**Strategic Goal 3:** Deliver economic, environmental, and social justice advancements through increased geothermal technology deployment.